



## Original Research Article

# Programming Adsorptive Removal of Organic Azo Dye from Aqueous Media Using Magnetic Carbon Nano-Composite

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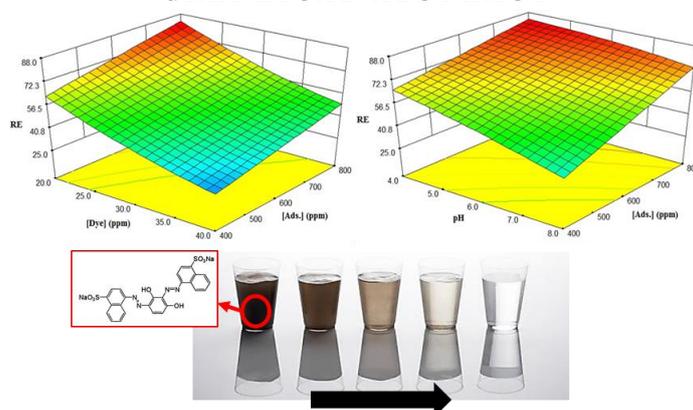
Optimization

Modeling

## ABSTRACT

In this research, the removal efficiency of an Acid Brown-14 as azo dye was carried out by an adsorbing method using a magnetic-activated carbon adsorbent, through which separation of adsorbent could be performed by a magnet at the end of the process. A second-order reduced polynomial model is used for method and optimization. Based on the model foresight, the process can remove the dye up to 82 % under the optimum situations of the primary pH = 4.6, [Dye] = 20 ppm, and [Ads.] = 791 ppm at room temperature. An experimentally accurate assessment of the model revealed that the model has a good agreement with the model prediction.

## GRAPHICAL ABSTRACT



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## Introduction

The fast development of textile manufacturing in recent decades has made synthetic dyes one of the main pollutants in water resources [1]. Besides, synthetic dyes are extensively used in industrial products such as cosmetics, leather, printing, food preparation, plastic and paper, and pigment [2]. Studies indicate that about  $7 \times 10^5$  tons of dye are produced annually throughout the world, of which about 10 to 15% of the total dye produced enters the environment without any treatment process [3]. Also, 70% of all dyes manufactured in the world are azo dyes, which are difficult to decompose due to the aromatic rings, toxicity, mutagenicity, and carcinogenicity [4, 5]. Several methods, including electrical coagulation, electrical oxidation, advanced oxidation, and adsorption, have been used to remove color contaminants from the aqueous medium [6-8]. Activated carbon has been considered by many researchers as a powerful adsorbent for the removal of various pollutants. This is also broadly used in the industry because of its low cost. The use of activated carbon in suspension is highly efficient, but its separation in the environment after the adsorption process is rather complicated and costly. To overcome this issue, the adsorbent can be used as a fixed bed form, but the main difficulty is decreasing the surface area. Recently, using magnetic adsorbent as a new adsorbent has been studied by scientists [9, 10]. For magnetization of an adsorbent, a magnetic core structured has to be entered into the adsorbent. Due to Magnetite's paramagnetic feature, it has been broadly used as a magnetic core [11]. To remove organic and inorganic pollutants, activated carbon has been widely used as adsorbent [12, 13]. So, magnetization of activated carbon can produce a good magnetic adsorbent which can be easily departed at the end of the process by a magnet.

This work aims to remove a textile dye from an aqueous medium by a low-priced and useful adsorption method on magnetically activated carbon adsorbents. Activated carbon is simply separated from the water at the end of the work

by using a magnet. In the light of the above concerns, the impact of parameters such as pH, adsorbent, primary dye molarity on the elimination efficiency of the dye has been studied and optimized.

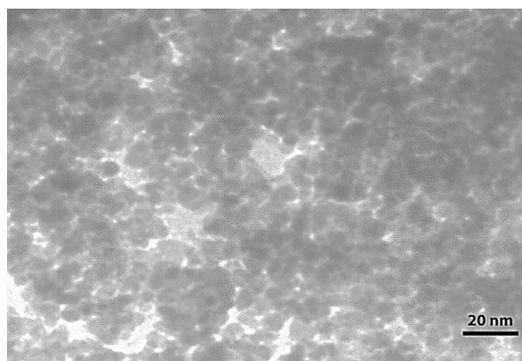
## Material and methods

### Reagents and instruments

The azo dye of Acid Brown 14,  $C_{26}H_{16}N_4Na_2O_8S_2$  with a molecular weight of 622.42 g/mol as a regular pollutant was purchased from AlvanSabet Company (Iran).  $FeCl_3 \cdot 6H_2O$ ,  $FeCl_2 \cdot 4H_2O$ , and ammonia solution (25%) were bought to make adsorbents. Sodium hydroxide and Sulfuric acid were used to set solution pH. All the substances were Merck and Fluka products. In each of the experiments, deionized water was used to prepare solutions. The concentration of the dye was measured by a UV-Vis spectrophotometer (Perkin Elmer Lambda 25). The structure of magnetic Nano-adsorbent was analyzed by Transmission Electron Microscope (TEM) (EM10C-100 KV).

### Synthesis of the Magnetic Nano-adsorbent

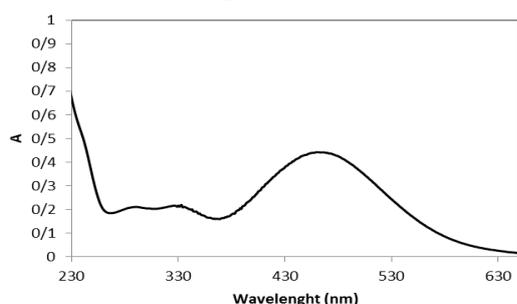
Because of the superparamagnetic aspect of magnetite, it was selected for the magnetization of activated carbon [11]. To prepare the magnetite nanoparticles, nitrogen gas was purged into 50 ml deionized water to deoxygenate it. Then, 1 g of activated carbon was added to the solution, and after well mixing, 0.79 g of  $FeCl_3 \cdot 6H_2O$  and 0.29 g of  $FeCl_2 \cdot 4H_2O$  were added and stirred again. Then, 3 mL of ammonia solution (25 wt. %) was added dropwise into the solution, and stirred continuously for 30 min. Notably, the solution was bubbled with nitrogen gas in all of the synthesis stages. Finally, the concerned magnetic activated carbon was washed several times using deionized water and ethanol and dried under vacuum at 60 °C for 5 h [14]. TEM analysis was used to characterize synthesized magnetic activated carbon. The relevant image of the magnetic adsorbent has been depicted in Figure 1.



**Figure 1:** TEM images of magnetic carbon Nano-composite

### Procedure

To investigate the removal process of the dye by the adsorption process, a specific concentration of the dye solution was provided, and a certain amount of magnetic adsorbent was added. In each test, 50 ml of solution with a certain dye concentration were prepared, and then a specific amount of adsorbent was added to the solution. After a specific stirring time by the magnetic stirrer, the adsorbent was removed using a magnet. Then, to measure the effectiveness of the process and calculate the amount of contaminant removal, the residual concentration of dye in the solution was measured spectroscopically at a maximum wavelength of 455 nm. UV-Vis spectrum of Acid brown 14 dye has been demonstrated in Figure 2.



**Figure 2:** UV-Vis spectrum of acid brown 14

### Design of the experiments

Optimization means determining a specific value for the parameters affecting the system in which we have the best response. After determining the variables affecting the process, these variables must be optimized. The two most common methods used in laboratory studies to determine

the optimal conditions are the classical method and statistical design. In the classical method, in addition to spending time and cost, the interferences are not known. Also in this method, the factors must be independent of each other. In recent years, researchers have considered the statistical design method for process optimization so that they can examine all aspects of the work by performing the least possible experiments and provide appropriate answers schematically and statistically through accurate calculations. One of the most effective methods in this field is the experimental design method. This method was first developed by Fisher and Yates in 1920 [15]. To design and perform experiments, the most widely used method is the response level method. In recent years, in studies related to wastewater and water purification, this method has received much attention [16, 17].

Experiments designed by the CCD method consists of three points: Cubic, axial, and center points. The total number of experiments (N) designed by the method can be determined as follows [18]:

$$N = 2^k + 2k + N_0 \quad (1)$$

where k, 2k, 2k, and N<sub>0</sub> are the number of factors, the term of cubic points, the term of axial points, and the term of center points, respectively.

In this research, optimization of the three important factors of adsorbent dosage, solution pH, and initial dye concentration were performed with considering maximizing removal efficiency of the dye as the response factor by central composite design (CCD).

## Result and Dissection

### Experimental Design and statistical analysis

At this stage, according to the results of the initial tests and review of studies conducted in this field, the practical variables and their range were identified. For this purpose, the amount of adsorbent, the primary pH of the solution, and the primary concentration of the sample factors were chosen as operational effective variables,

and the removal competence was selected as the response. Each parameter in this study was studied at five different levels with code values of  $-\alpha$ ,  $-1$ ,  $0$ ,  $1$ ,  $+\alpha$ . Table 1 shows the varieties and levels of the independent variable parameters used along with the CCD matrix as well as designed experiments and related experimental answers. To find the best model, after examining and evaluating the fit defects related to different models, a quadratic model was recommended by the software to explain the process. The proposed model was analyzed by study of variance (ANOVA), which is presented in Table 2. An F-value of 238.83 and a P-value of 0.0001 indicate that the proposed model is important for simulating the adsorption process of the dye by magnetic-activated carbon. The proposed model for the system includes three terms of single-component or linear effects (A, B, C), three terms of dual or interaction effects (AB, AC, BC), and three terms of quadratic effects (A<sup>2</sup>, B<sup>2</sup>, C<sup>2</sup>). However, not all of these parameters have a meaningful effect on the model and should be removed. Values less than 0.05 and greater than 0.1 for the P-value parameter belonging to each

$$RE = 158.6 - 11.11 \text{ pH} - 4.43 [\text{Dye}] - 0.00074 [\text{Ads.}] + 0.219 \text{ pH} [\text{Dye}] - 0.011 \text{ pH} [\text{Ads.}] - 0.365 \text{ pH}^2 + 0.029 [\text{Dye}]^2 \quad (2)$$

term of the model, respectively, indicate whether those terms are important or unimportant in the model [19].

In the recommended model, the "P-value" parameter is important for all expressions related to linear and quadratic terms, and interactive terms are irrelevant. Also, the F-value equal to 4.59 for the parameter Lack of Fit shows that the lack of fit is not notable. The sum of the squares  $R^2 = 0.99$  indicates that the model has great exactness. On the other side, the "Pred R-Squared" of 0.98 and "Adj R-Squared" of 0.97 represent the model predict the response as well. Also, the parameter of "Adeq Precision" indicates the signal-to-noise ratio, in which a ratio bigger than 4 is acceptable; in any case this parameter is equal to 53.97, which is a desirable value.

After statistical analysis, the proposed model was presented as a quadratic equation in terms of actual parameters by the software, which is shown in Equation (2). This mathematical equation presents the removal rate of the dye by magnetically activated carbon as a function of the value of various operating parameters.

**Table 1:** The range of variables and designed experiments by CCD with related experimental responses

Variables	Range and level				
	$-\alpha$	$-1$	$0$	$+1$	$+\alpha$
A: pH	2.6	4	6	8	9.4
B: [Dye](ppm)	13.2	20	30	40	46.8
C: [Ads.] (ppm)	263.6	400	600	800	936.3
Design Matrix					
Runs	The factors			Removal Efficiency (RE)	
	pH	[Dye](ppm)	[Ads.] (ppm)		
1	6.0	30.0	600.0	51.2	
2	6.0	46.8	600.0	37.5	
3	9.4	30.0	600.0	40.1	
4	6.0	30.0	600.0	50.5	
5	4.0	20.0	400.0	69.3	
6	6.0	30.0	600.0	50.2	
7	4.0	40.0	400.0	28.4	
8	6.0	30.0	600.0	48.8	
9	6.0	30.0	600.0	51.0	
10	4.0	20.0	800.0	81.4	
11	8.0	20.0	800.0	74.5	
12	8.0	20.0	400.0	38.5	
13	6.0	13.2	600.0	81.6	

14	8.0	40.0	800.0	54.5
15	2.6	30.0	600.0	54.0
16	6.0	30.0	600.0	51.8
17	6.0	30.0	263.6	30.0
18	8.0	40.0	400.0	21.5
19	4.0	40.0	800.0	50.2
20	6.0	30.0	936.4	74.5

**Table 2:** Analysis of variance for the response surface reduced quadratic model

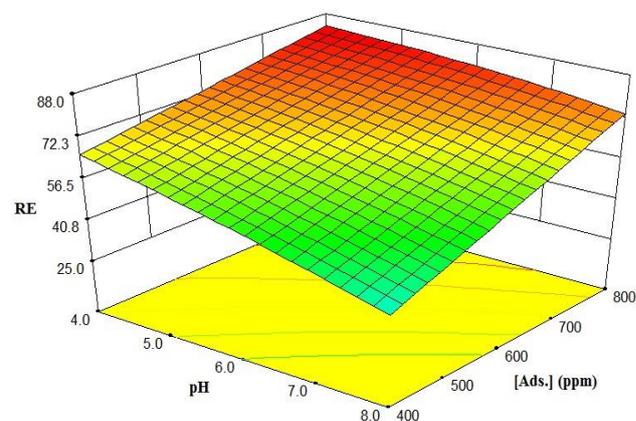
Source	Sum of Squares	df	Mean Square	F-Value	p-value Prob> F
Model	5548.69	7	792.67	238.83	< 0.0001
A-pH	296.90	1	296.90	89.46	< 0.0001
B-Dye	2459.34	1	2459.34	740.99	< 0.0001
C-Ads	2313.23	1	2313.23	696.97	< 0.0001
AB	154.00	1	154.00	46.40	< 0.0001
AC	154.00	1	154.00	46.40	< 0.0001
A <sup>2</sup>	31.06	1	31.06	9.36	< 0.0001
B <sup>2</sup>	127.39	1	127.39	38.38	< 0.0001
Residual	39.83	12	3.32		
Lack of Fit	34.46	7	4.92	4.59	0.0564
Pure Error	5.37	5	1.07		
Cor Total	5588.52	19			

#### *Effect of operational parameters and process optimization*

To study how each variable is affected and the interaction or dual effects of the variables on the response generated by the model, three-dimensional plots based on the polynomial function of the model were prepared using experimental design software. In these plots, the two variables change in the experimental range, while the other parameters are kept constant.

Figure 3 shows a three-dimensional diagram of the dye removal efficiency using magnetic-activated carbon as a function of the pH and amount of adsorbent dosage. It is observed that with increasing the amount of adsorbent and decreasing the pH, the removal efficiency increases. By decreasing the pH, the positive charge of the adsorbent surface increases, and its tendency to the dye increases. Also, with raising the amount of adsorbent, the number of active sites for the adsorption of pollutants increases,

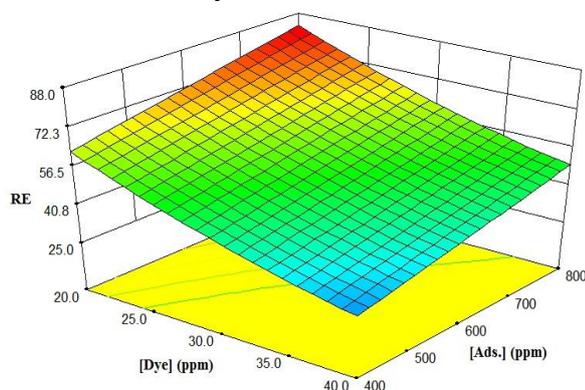
and as a result, the removal efficiency of dye increases.



**Figure 3:** The 3D plot presenting the effect of pH and amount of adsorbent in the dye removal efficiency

Figure 4 confirms the response surface plot for the dye removal efficiency as a function of the initial dye concentration and the amount of adsorbent used. As can be noticed, the removal effectiveness decreases with increasing the initial concentration of the dye. As the amount of

contaminant increases, more adsorbent is required, and by using a certain amount of adsorbent that has a special active surface and increasing the concentration of contaminant, the removal efficiency will decrease.



**Figure 4:** The 3D plot presenting the effect of dye initial concentration and the amount of adsorbent in the dye removal efficiency

Model optimization and finding the optimal value of variables in the dye removal process based on the utility function was performed by the software. For this purpose, in the software, optimization conditions related to each variable and the importance of each were determined. In general, the range of parameters in the design and response range was set to the maximum value. After performing the optimization process, the software predicted 82% removal efficiency using [Ads.] = 791 ppm, pH = 4.6, and [Dye] = 20 ppm after 60 min. To check the accuracy of the model prediction, an experiment was performed under the mentioned optimal conditions, which experimentally obtained 78% efficiency. It can be seen that the result of the experimental test is in good agreement with the model prediction.

## Conclusion

Herein, elimination efficiency of an azo dye was carried out by an adsorption method using a magnetically activated carbon adsorbent. The tests were planned based on the CCD method and also the process was modeled. Briefly, the resulting notable data can be specified from this research. The process was formed and optimized by a second-order reduced polynomial model.

The adsorption process using magnetic carbon Nano-composite can remove the dye up to 82 % under the optimum situations of the primary pH = 4.6, [Dye] = 20 ppm, and [Ads.] = 791 ppm at room temperature.

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## Authors' contributions

All authors contributed toward data analysis, drafting and revising the paper and agreed to be responsible for all the aspects of this work.

## Conflict of Interest

We have no conflicts of interest to disclose.

## References

- [1]. Karimi A., Mahdizadeh F., Eskandarian M., *Chem. Indus. Chem. Eng. Q. CICEQ*, 2012, **18**:89 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [2]. (a) Li M., Li J.T., Sun H.W., *Ultrason. Sonochem.*, 2008, **15**:37 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (b) Khakyzadeh V., Wang Y.H., Breit B., *Chem. Commun.*, 2017, **53**:4966 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (c) Zolfigol M.A., Moosavi-Zare A.R., Arghavani-Hadi P., Zare A., Khakyzadeh V., Darvishi G., *RSCA dv.*, 2012, **2**:3618 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (d) Zolfigol M.A., Moosavi-Zare A.R., Moosavi P., Khakyzadeh V., Zare A., *Comptes. Rendus. Chimie.*, 2013, **16**:962 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (e) Moosavi-Zare A.R., Zolfigol M.A., Zarei M., Zare A., Khakyzadeh V., *J. Mol. Liq.*, 2015, **1**:373 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [3]. (a) Martínez S.S., Uribe E.V., *Ultrason. Sonochem.*, 2012, **19**:174 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (b) Tavoosi F., Movahedi M., Rasouli N., *Adv. J. Chem. A*, 2021, **4**:32 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (c) Olasehinde E., Abegunde S., *Adv. J. Chem. A*, 2020, **3**:663 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (d) Farhadi M., Sayyahi S., Gorjizadeh M., *Adv. J. Chem.*

- A, 2021, 4:188 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [4]. (a) Ghoneim M.M., El-Desoky H.S., Zidan N.M., *Desalination*, 2011, 274:22 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (b) Gaikwad S.V., Gaikwad M.V., Lokhande P.D., *J. Appl. Organomet. Chem.*, 2021, 1:1 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (c) Hote B.S., Muley D.B., Mandawad G.G., *J. Appl. Organomet. Chem.*, 2021, 1:9 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (d) R.A. Shinde, V.A. Adole, *J. Appl. Organomet. Chem.*, 2021, 1:48 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [5]. (a) Krishnakumar B., Swaminathan M., *Indian J. Chem.*, 2010, 49A:1035 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (b) Zargaran M., Zargar B., Rastegar Zadeh S., Andayesh R., *Adv. J. Chem. A*, 2020, 3:551 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)] (c) Mirbaloochzahi M., Rezvani A., Samimi A., Shayesteh M., *Adv. J. Chem. A*, 2020, 3:612 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [6]. Rezaei Vahidian H., Soleymani A.R., Basiri Parsa J., *Desalination Water Treat.*, 2015, 56:388 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [7]. Parsa J.B., Vahidian H.R., Soleymani A., Abbasi M., *Desalination*, 2011, 278:295 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [8]. Saien J., Asgari M., Soleymani A., Taghavinia N., *Chem. Eng. J.*, 2009, 151:295 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [9]. Zhang S., Niu H., Cai Y., Zhao X., Shi Y., *Chem. Eng. J.*, 2010, 158:599 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [10]. Ren Y., Li N., Feng J., Luan T., Wen Q., Li Z., Zhang M., *J. Colloid Interface Sci.*, 2012, 367:415 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [11]. Philipse A.P., Van Bruggen M.P., Pathmamanoharan C., *Langmuir*, 1994, 10:92 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [12]. Selvi K., Pattabhi S., Kadirvelu K., *Bioresour. Technol.*, 2001, 80:87 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [13]. Zarei A.R., Pedram A., Rezaeivahidian H., *Desalin. Water Treat.*, 2015, 57:18906 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [14]. Bastami T.R., Entezari M.H., *Chem. Eng. J.*, 2012, 210:510 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [15]. Hinkelmann K., Kempthorne O., *Design and Analysis of Experiments, Introduction to Experimental Design*, John Wiley & Sons, 2007 [[Google scholar](#)], [[Publisher](#)]
- [16]. Ahmadi M., Vahabzadeh F., Bonakdarpour B., Mofarrah E., Mehranian M., *J. Hazard. Mater.*, 2005, 123:187 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [17]. Guaracho V., Kaminari N., Ponte M., Ponte H., *J. Hazard. Mater.*, 2009, 172:1087 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [18]. Zarei A.R., Rezaeivahidian H., Soleymani A.R., *Process Saf. Environ. Prot.*, 2015, 98:109 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]
- [19]. Sakkas V.A., Islam M.A., Stalikas C., Albanis T.A., *J. Hazard. Mater.*, 2010, 175:33 [[Crossref](#)], [[Google scholar](#)], [[Publisher](#)]

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